

245th ECS Meeting, San Francisco CA

**I01-1893 - Enhancing Efficiency and Durability
of PEM Water Electrolysis with Low Iridium
Loading through Nanofiber-Modified Porous
Transport Electrodes**

Xin Wen, Bastien Penninckx, Sankar Sasidharan, Ellinor Ehrnberg, Fabian Wenger

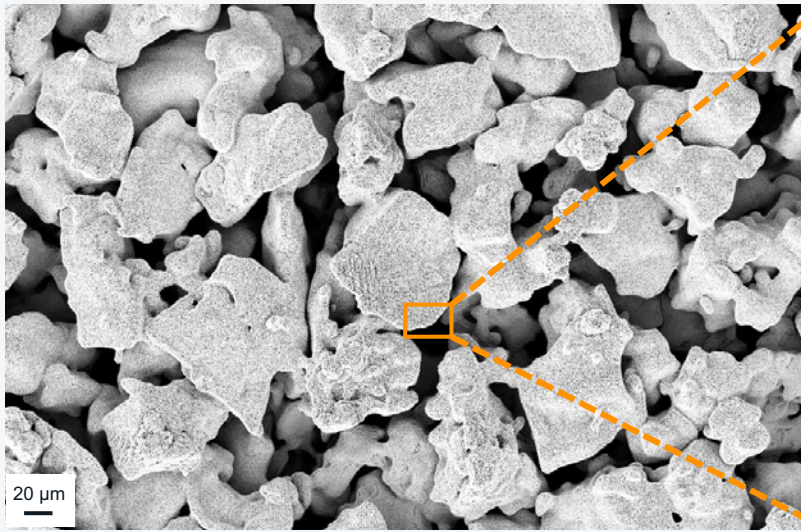
Smoltek Hydrogen AB, Gothenburg, Sweden

2024-05-30

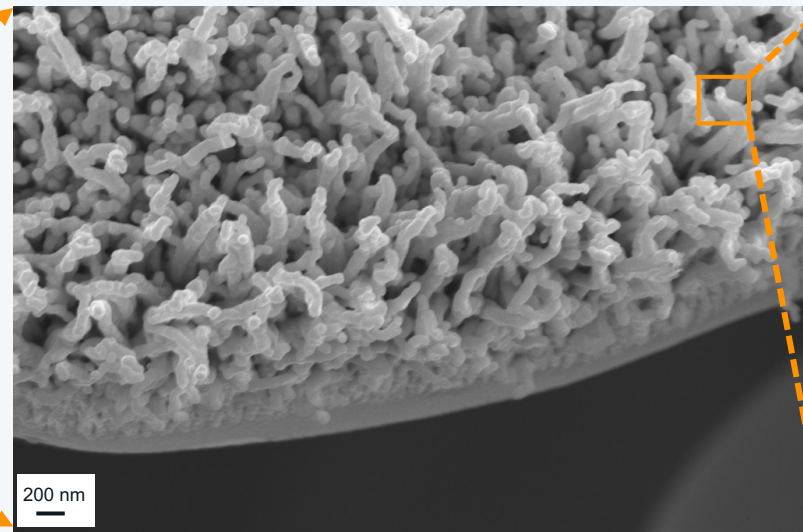




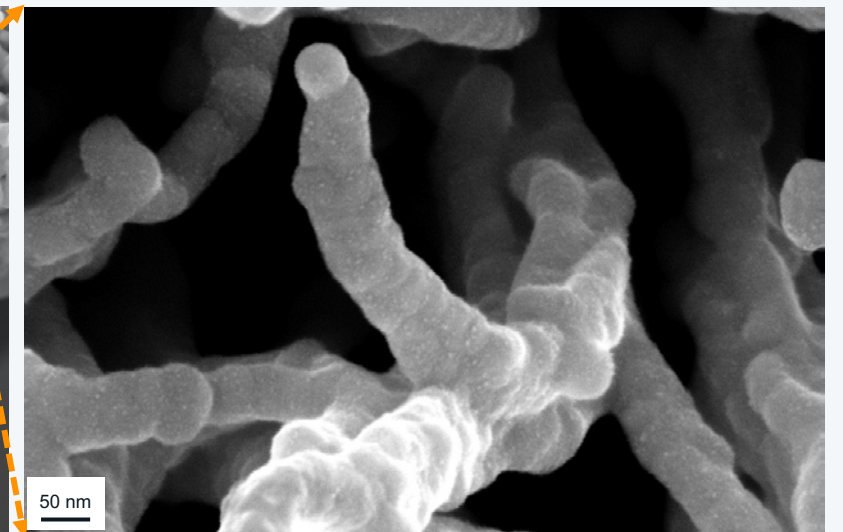
- Unlock 10 GW-manufacturing scale-up for PEM water electrolyzers
- Durable performance at iridium loading below 0.2 mg/cm²
- Porous transport electrode (PTE) with enhanced surface area
- Cost-efficient supply chain for all volume processing steps for PTE



Porous transport electrode



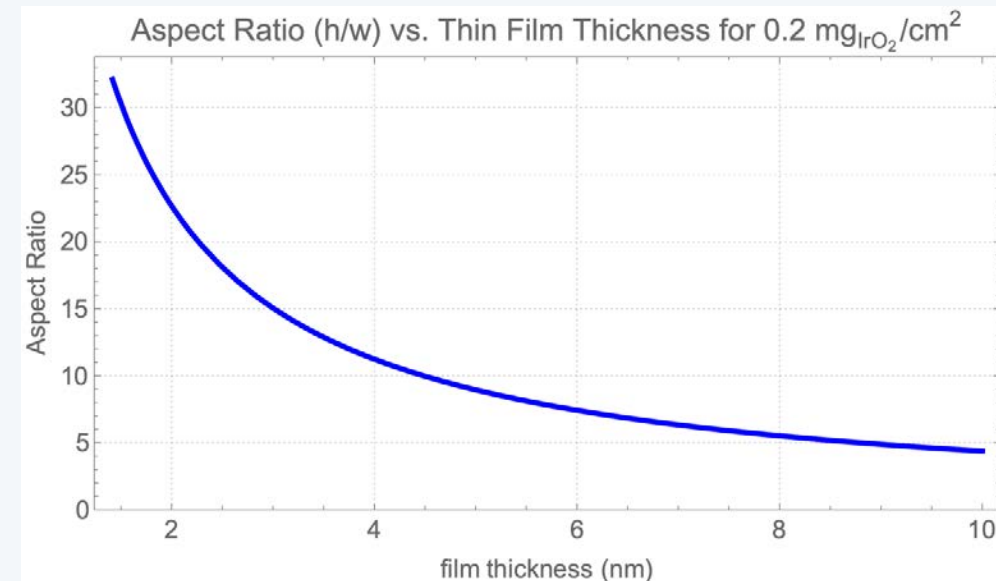
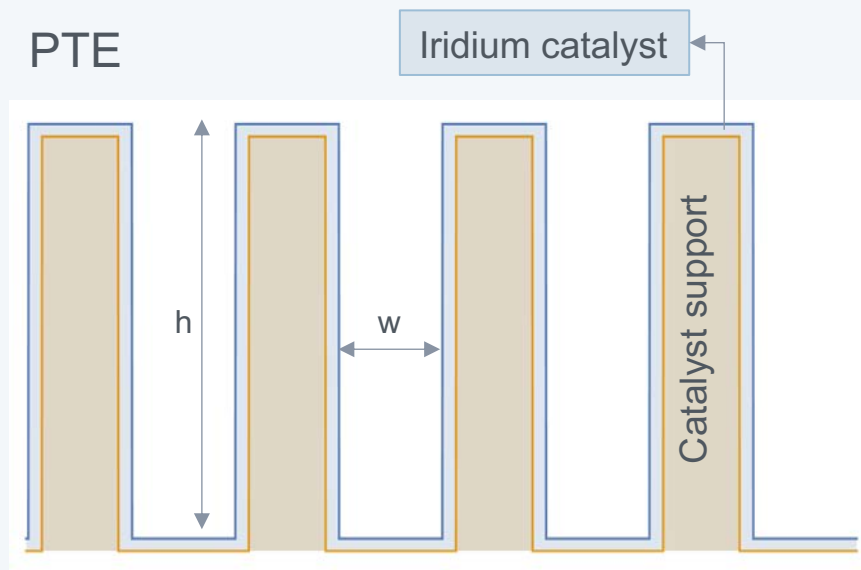
Enhanced surface area

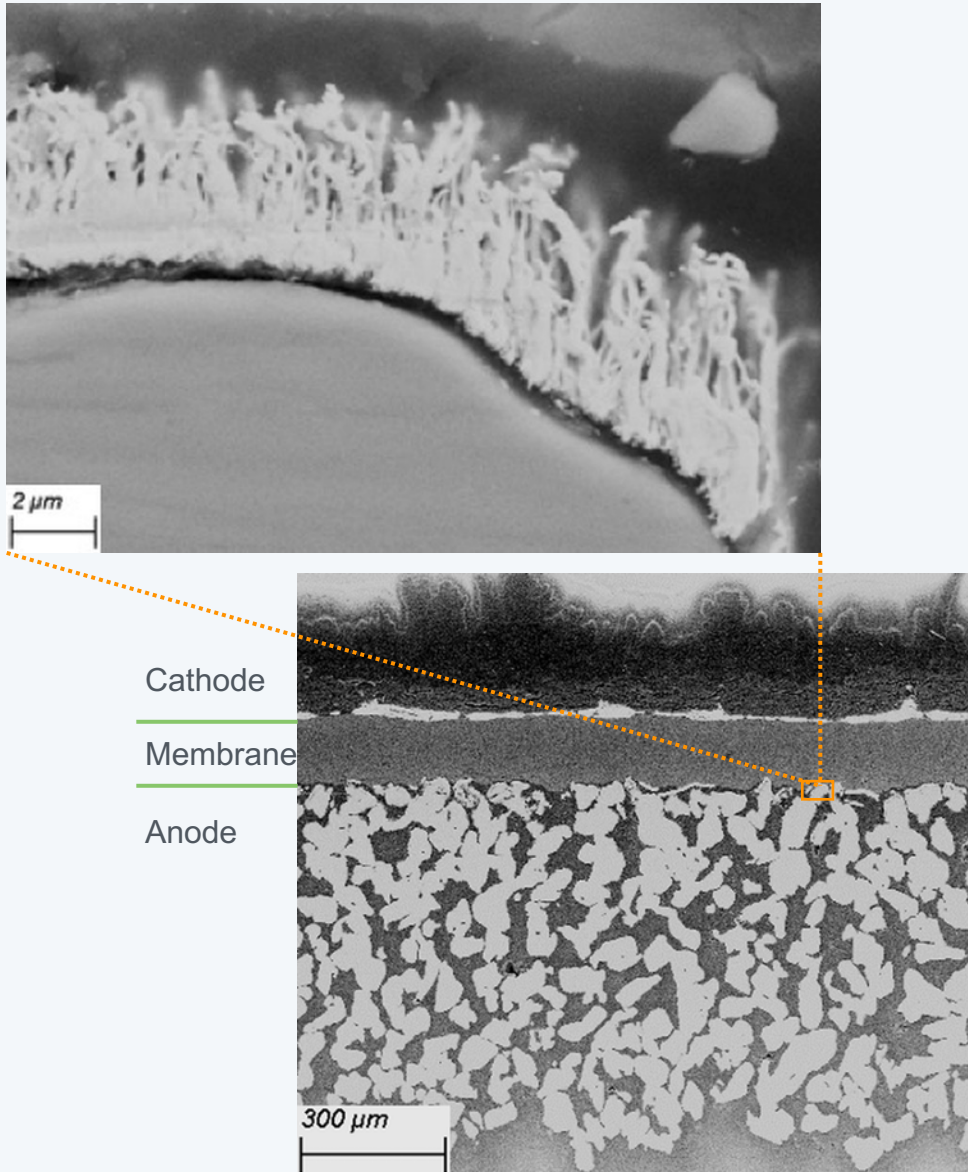


Coated nanostructure



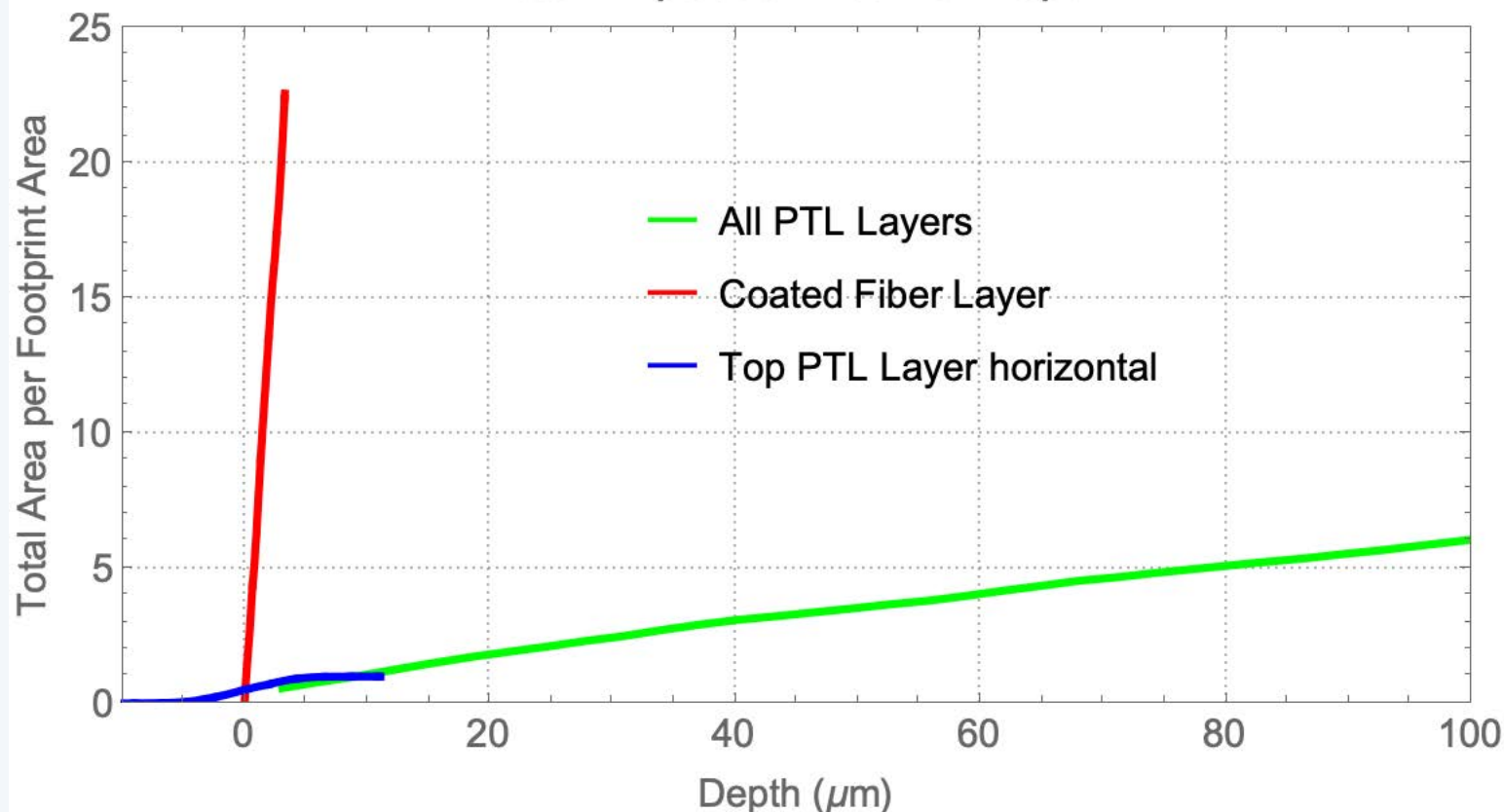
- Unlock 10 GW-manufacturing scale-up for PEM water electrolyzers
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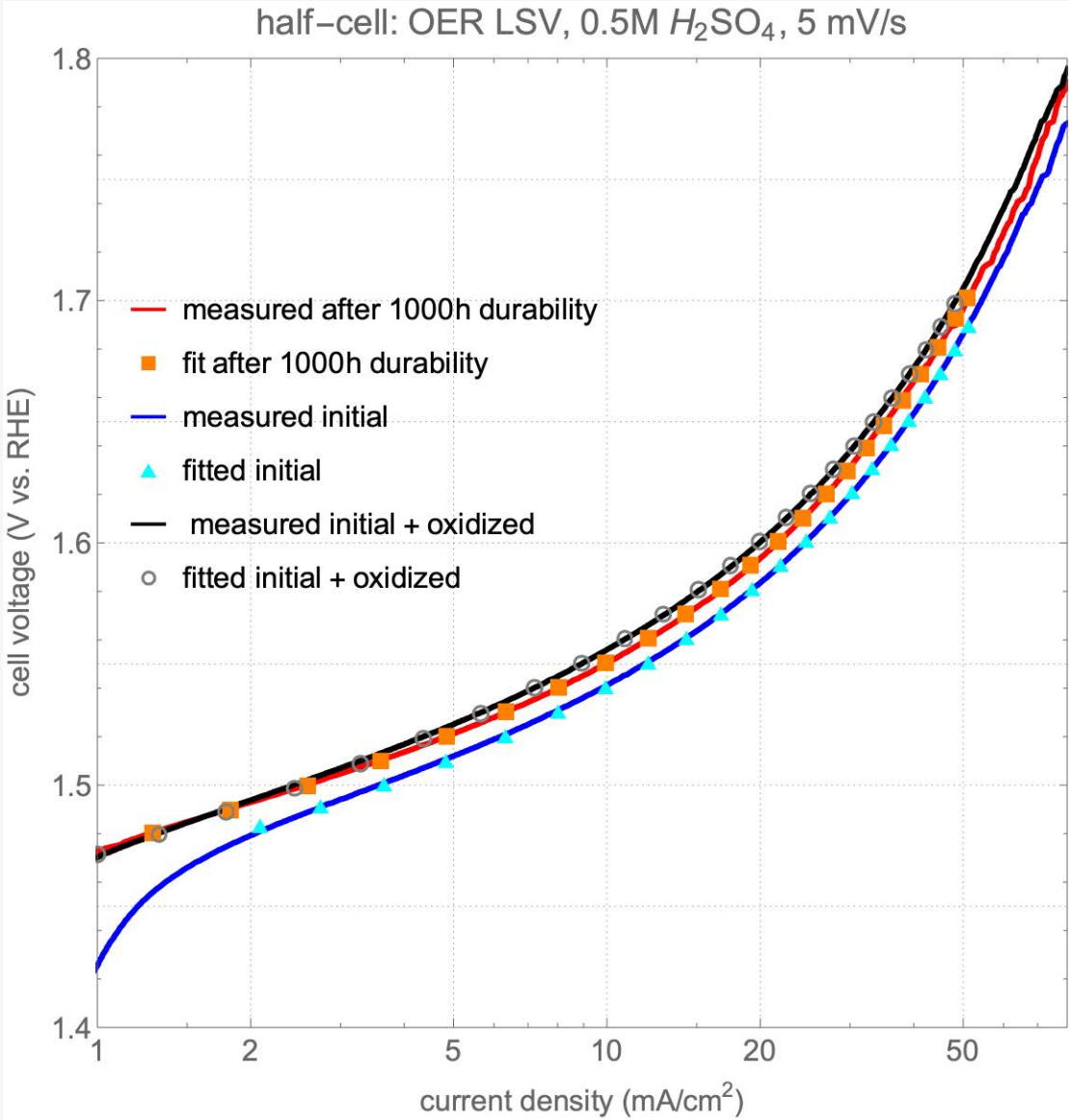
- **Tolerates up to 2.6 V @ 2A/cm² for 1000 hours**
- PTE Anode:
 - **3...10 μm vertical nanofiber, 100...150 nm thick, 20...50% porosity**
 - Graphitic core, ALD Pt coating 12...**25**...50 nm without pin holes
 - electrodeposited 6...20 nm porous Iridium nanoparticle layer
 - Iridium loading 0.1...**0.2**...0.7 mg/cm²,
Platinum loading 0.5...**1.1**...1.3 mg/cm²
- Ionomer drop coating and hot-pressing with Nafion 115
- Cathode: Generic (Fuel Cell Store)
- **Lab and A4 size prototypes**

Total Exposed Area vs. Depth



- **Nanofiber catalyst layer preserves proximity to membrane and metallic contact**
- A standard PTL will not expose enough area in close proximity even at low loadings

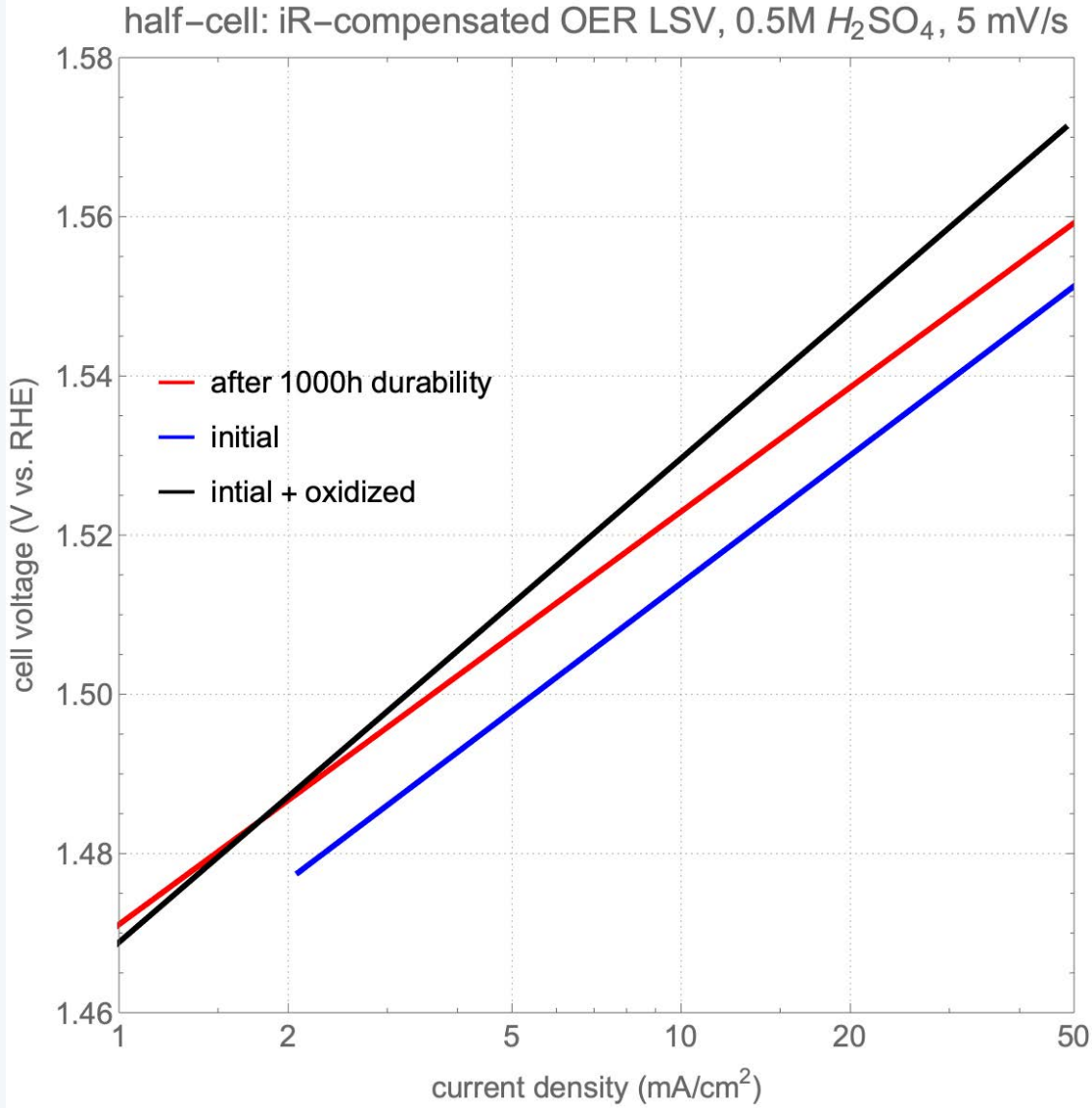
OER Half-Cell LSV: 1000 h Durability Test Anode Post-Mortem Activity Comparison (1/2)



- Most of the apparent irreversible loss of the full cell performance is recovered by subjecting the anode to half-cell OER environment again!
- PTE: all is well in half-cell
- $E = A + B \log_{10} j/j_0 + R j$

Parameter Fit	A (V)	B (mV/dec)	j_0 (mA/cm^2)	R (Ωcm^2)
1000h	1.47	52	1.12	2.8
initial	1.45	53	0.88	2.7
initial+ox	1.47	60	1.05	2.7

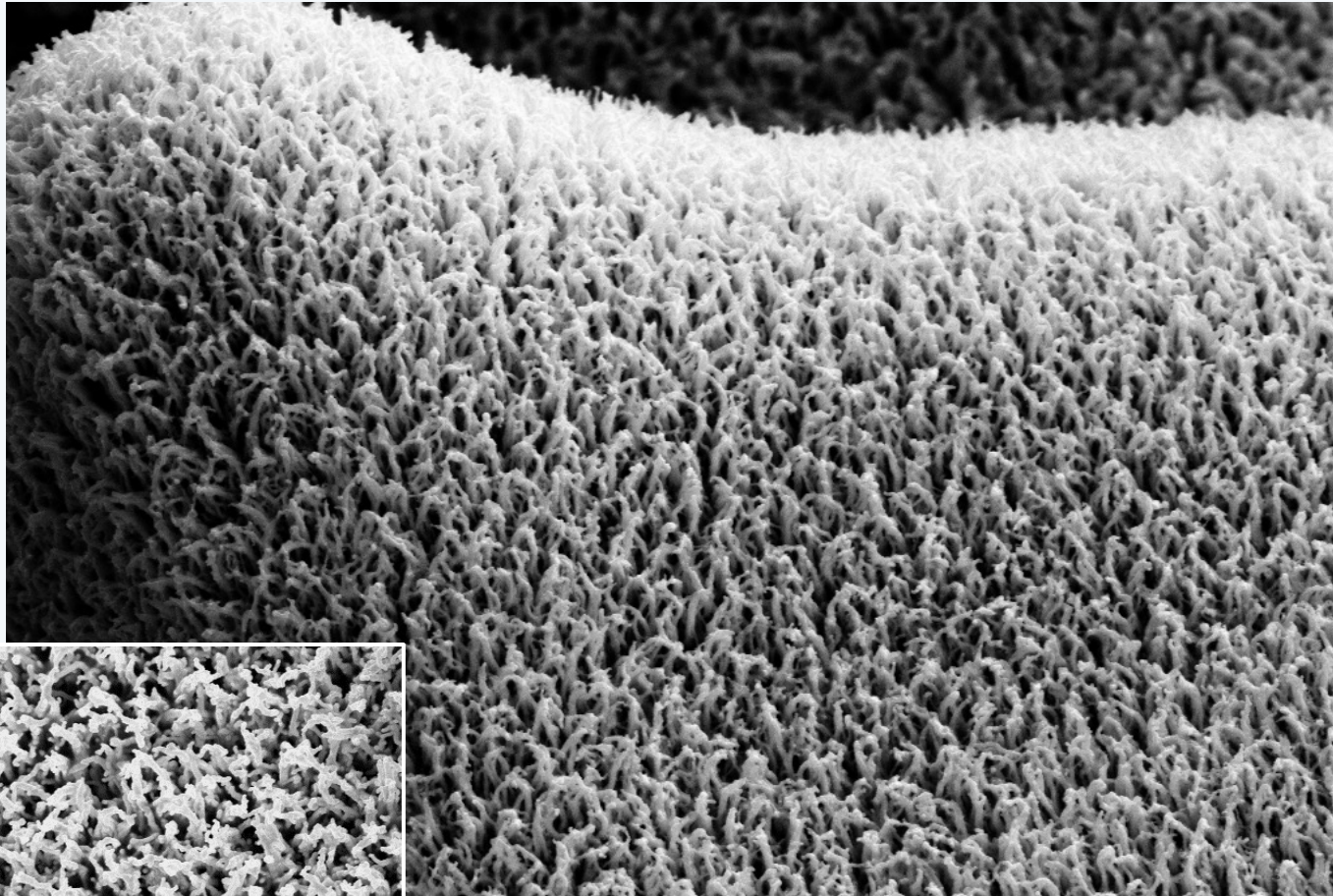
OER Half-Cell LSV: 1000 h Durability Test Anode Post-Mortem Activity Comparison (2/2)



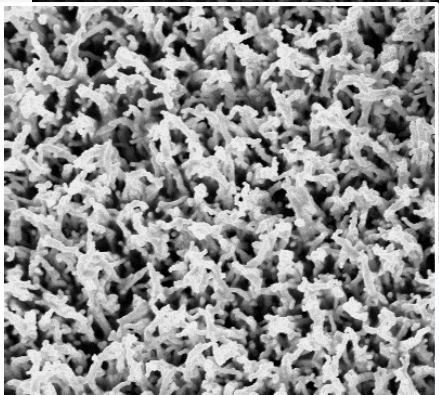
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After

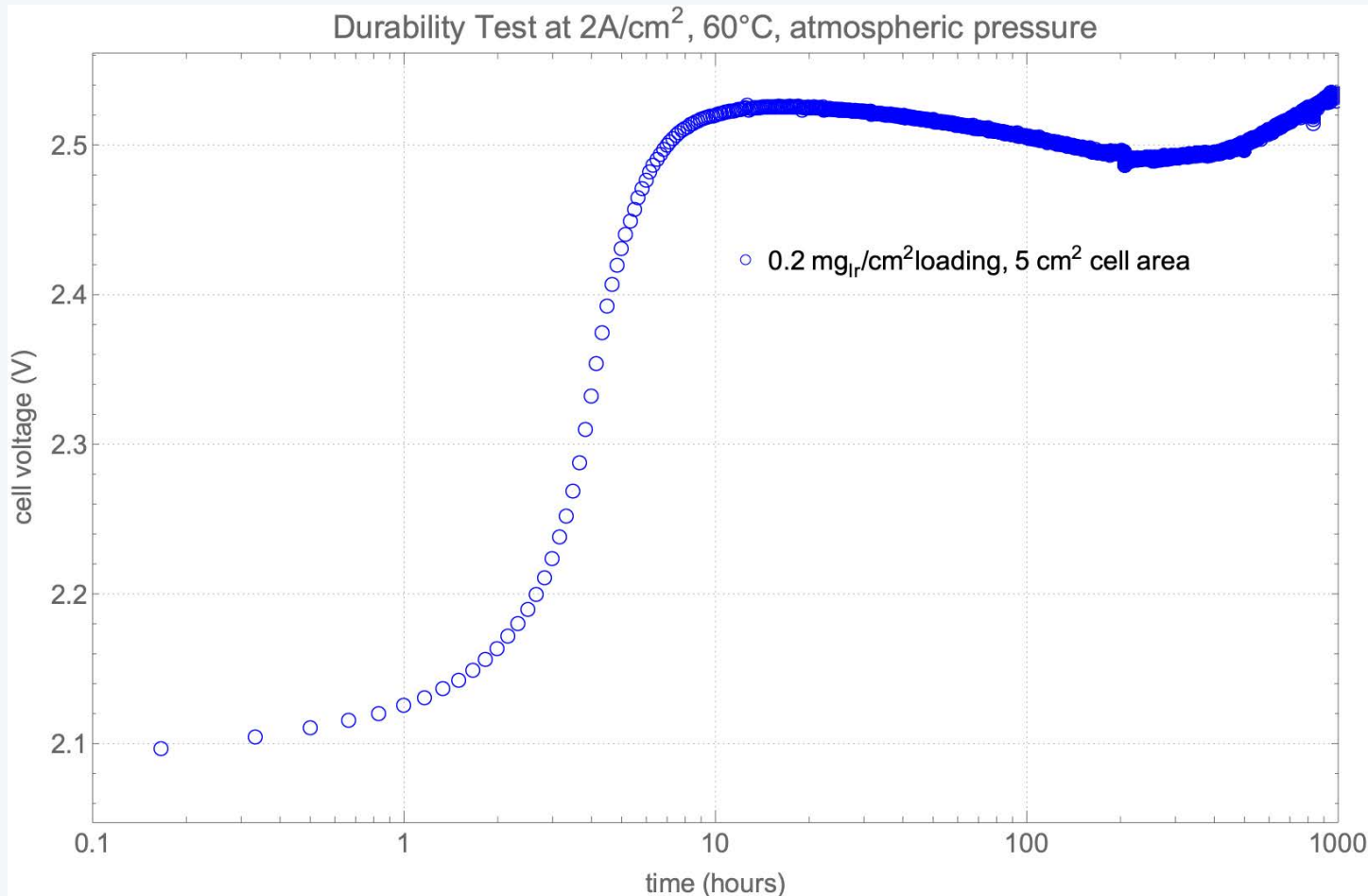


1 μm

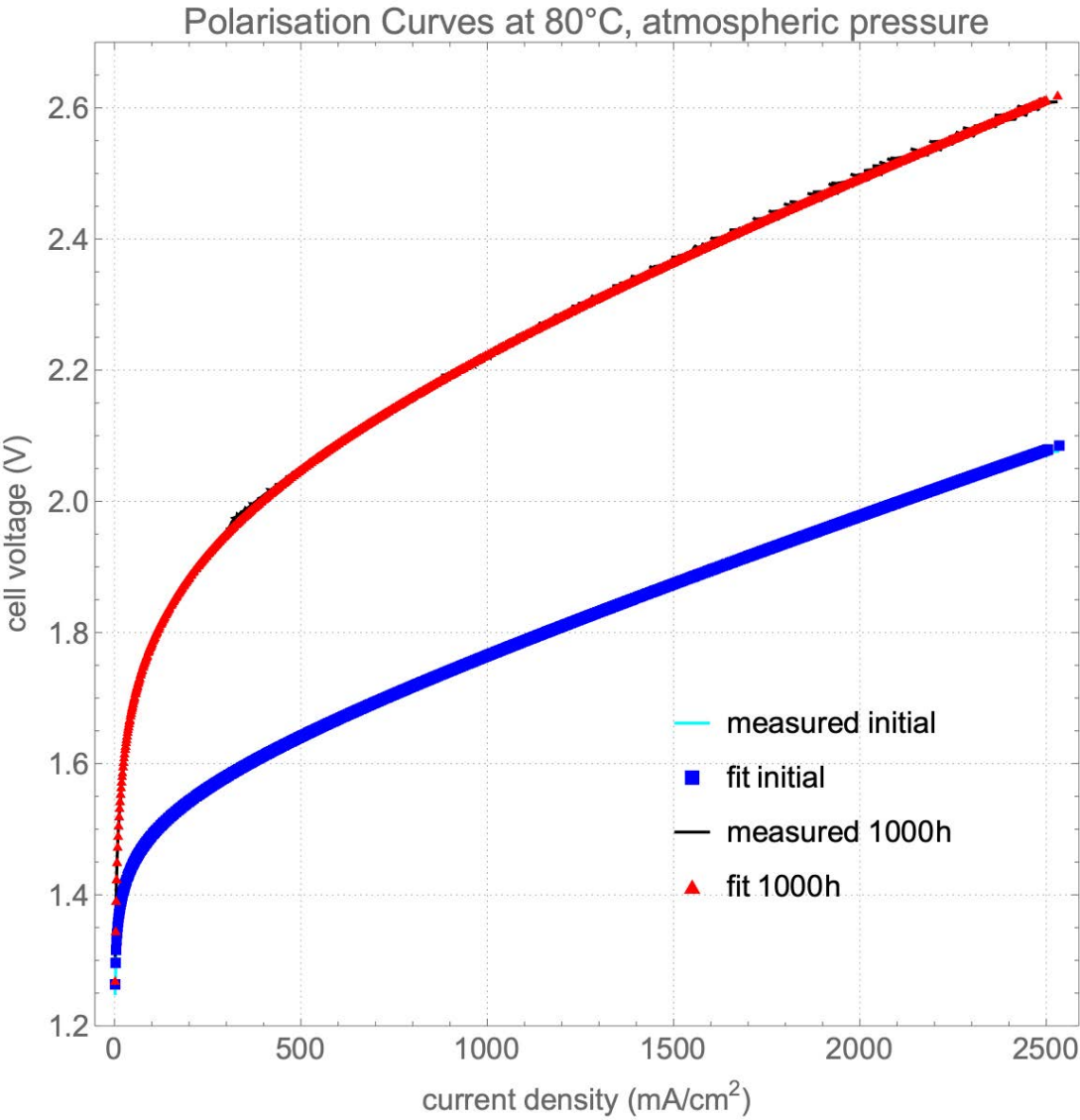


Before

- No degradation of fiber morphology
- Rapid increase of voltage the first 10h from 2 to 2.5V, then stable
- After cell disassembly the anode displays the activity of an initially electrochemically oxidized sample at same loading (see previous slides)
- All EIS and polarization data taken at 80°C, but test system limited to 60°C for long-term stability tests

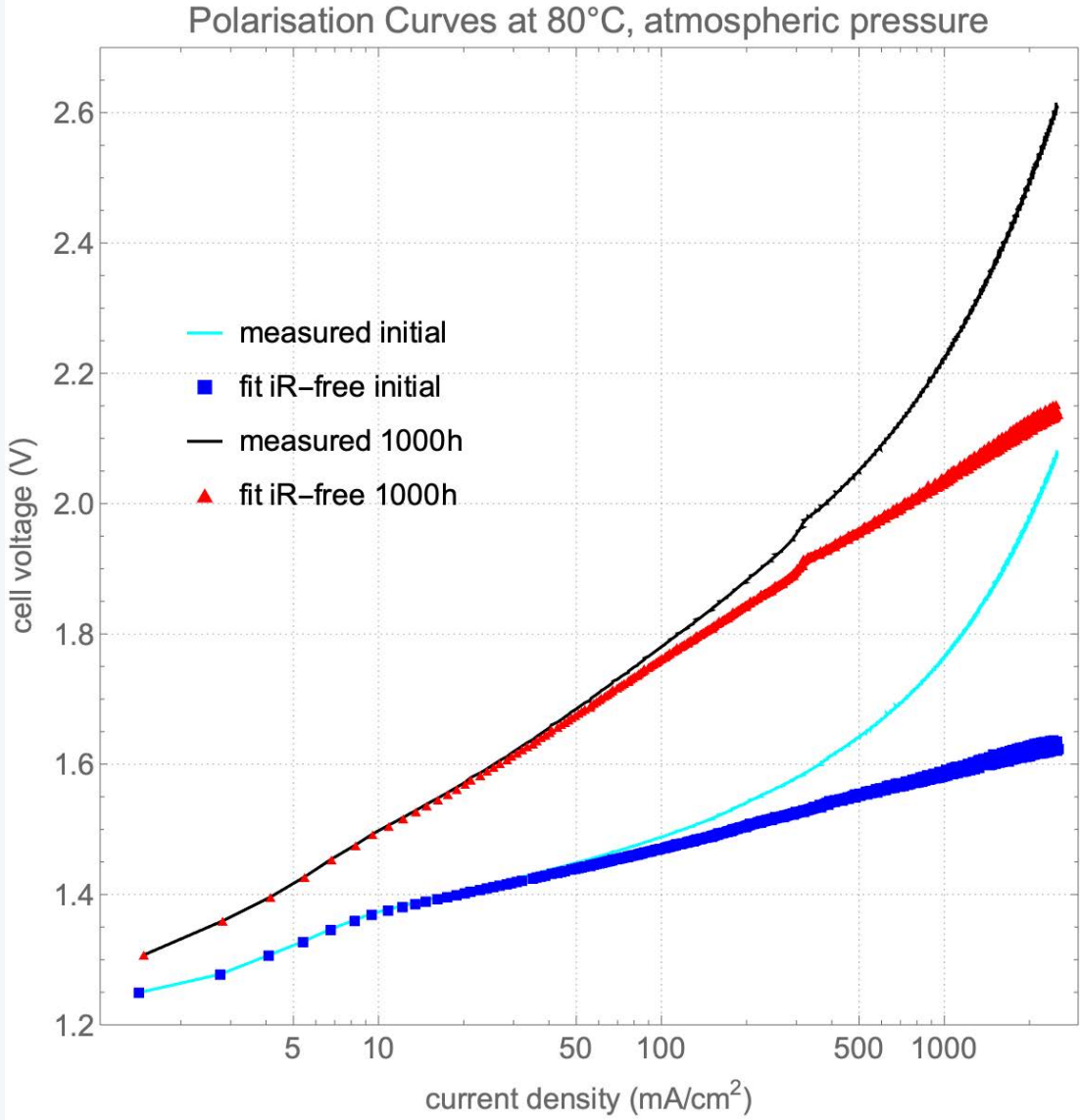


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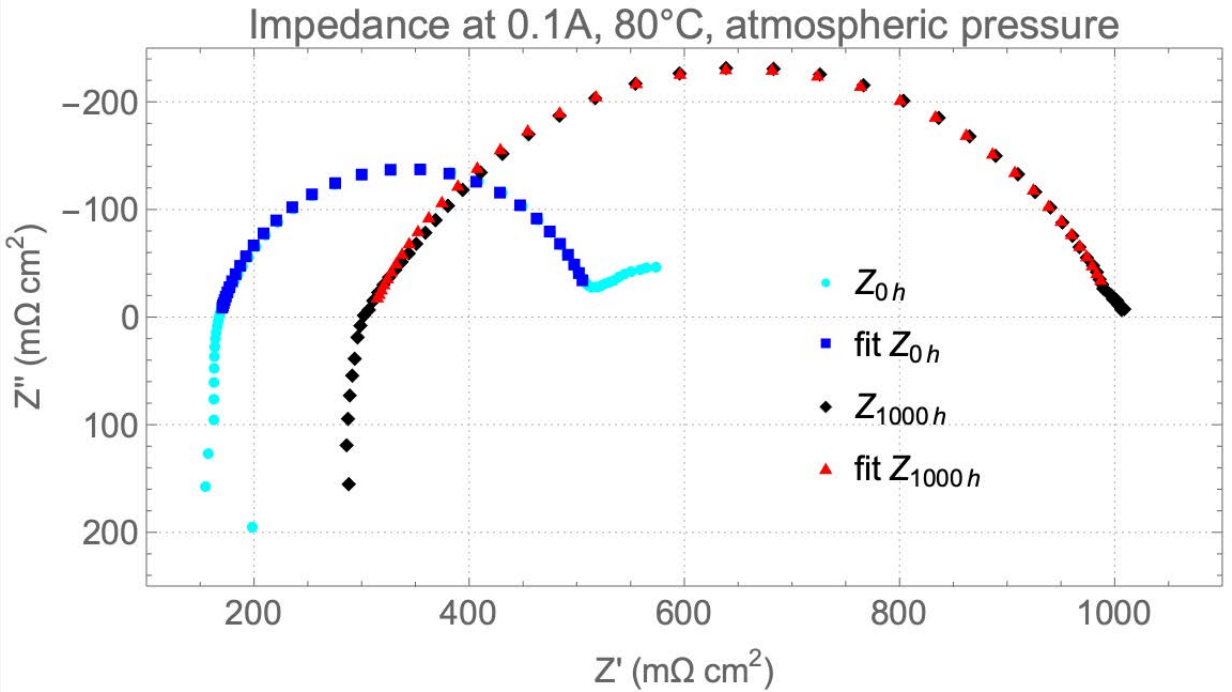
- High Tafel slopes
- $E = E_0 + B \log_{10} j/j_0 + R j$

Parameter Fit	E_0 (V)	B (mV/dec)	j_0 (mA/cm²)	R (mΩ cm²)
0h	1.25	113	1.17	179
1000h	1.23	271	1.14	187

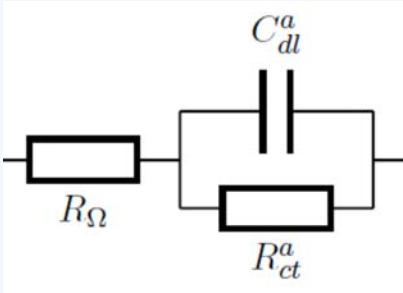


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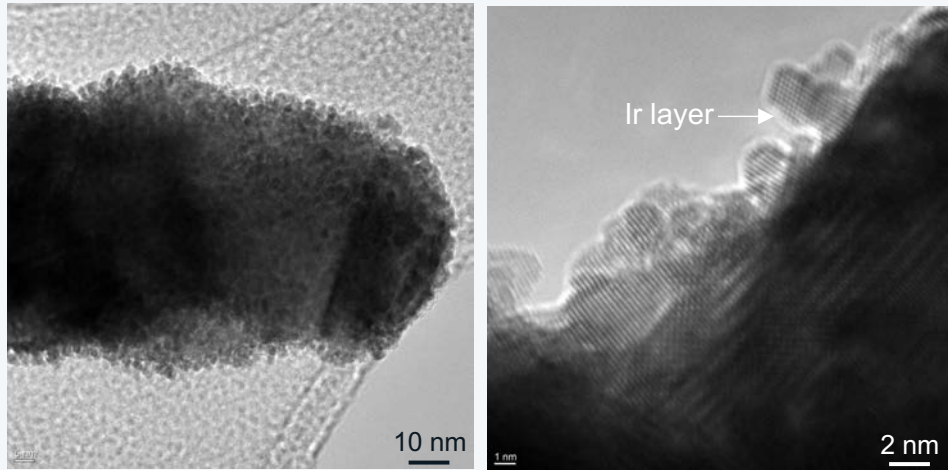


- EIS model simplified Randles circuit with CPE and non-linear fit of exponent in selected frequency interval

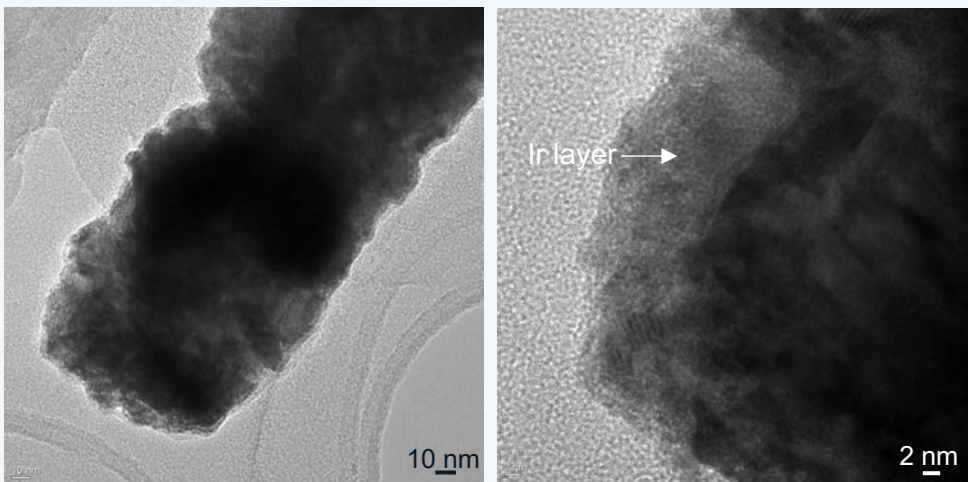


EIS @ 0.1A	HFR (mΩ cm ²)	R _{CT} (mΩ cm ²)	a	C _{CPE} (s ^{a-1} mF/cm ²)
0h	168	349	0.85	20
1000h	306	698	0.74	10

Before 1000h

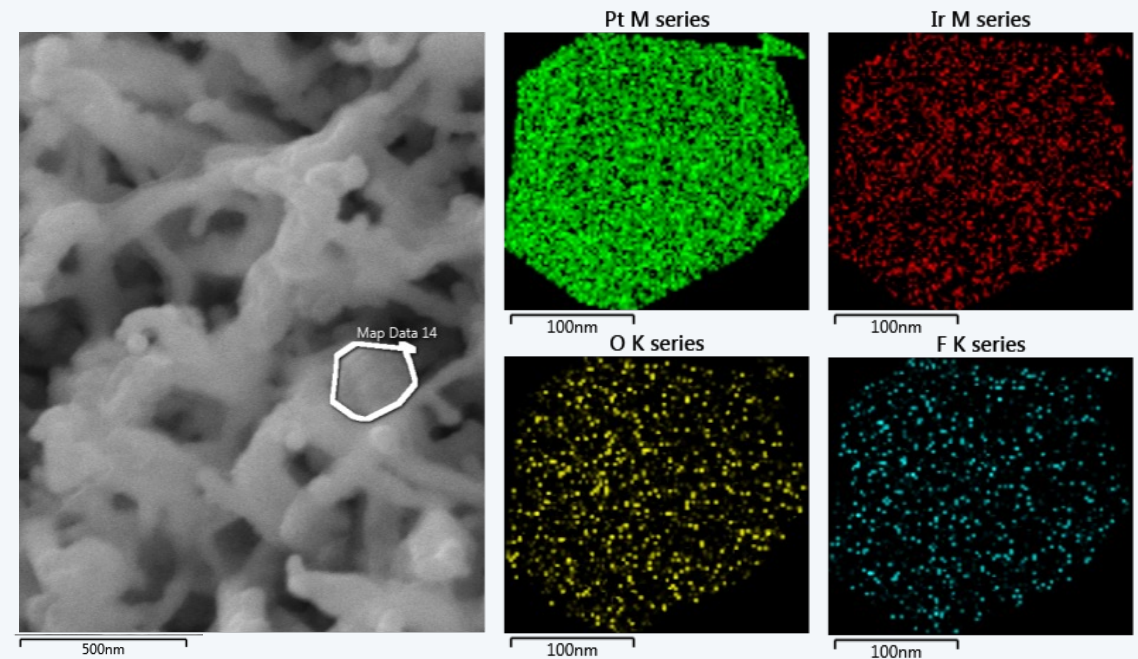


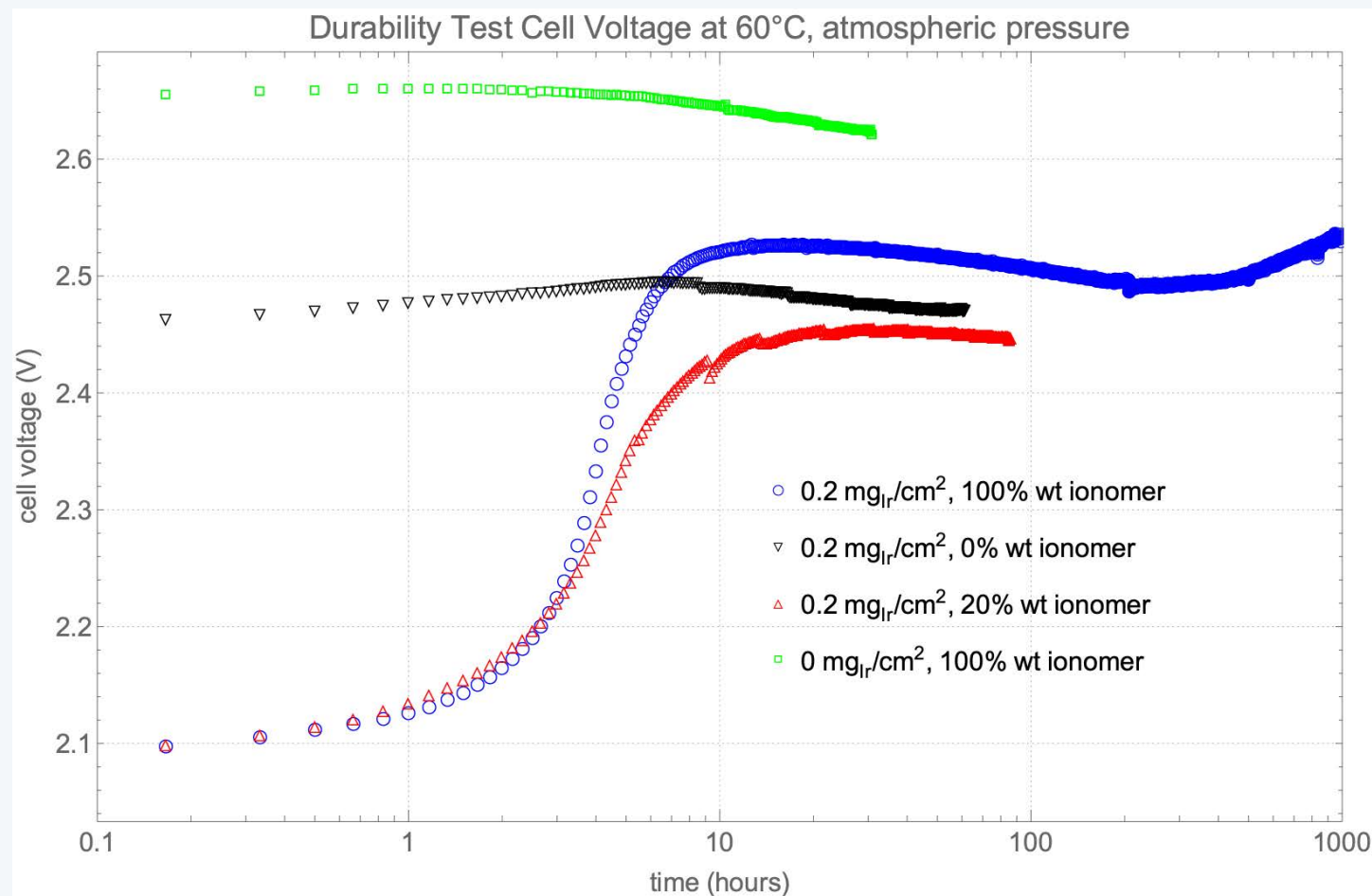
After 1000h



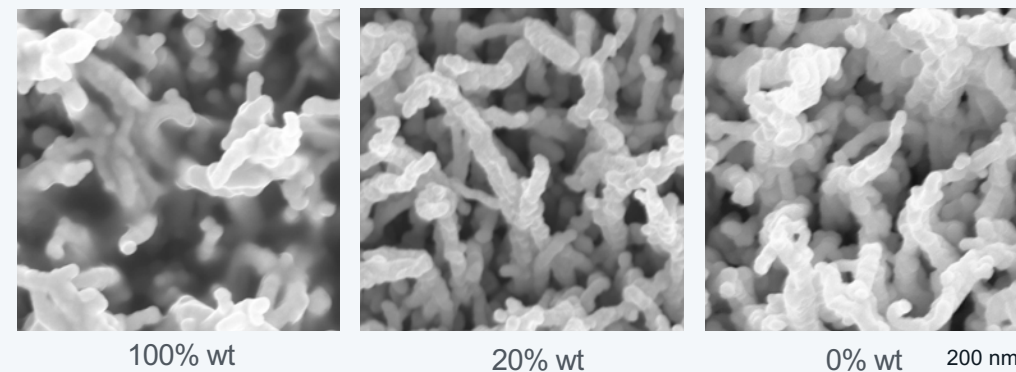
- Ir catalyst remained on the PTE after 1000h durability test but became less crystallized.

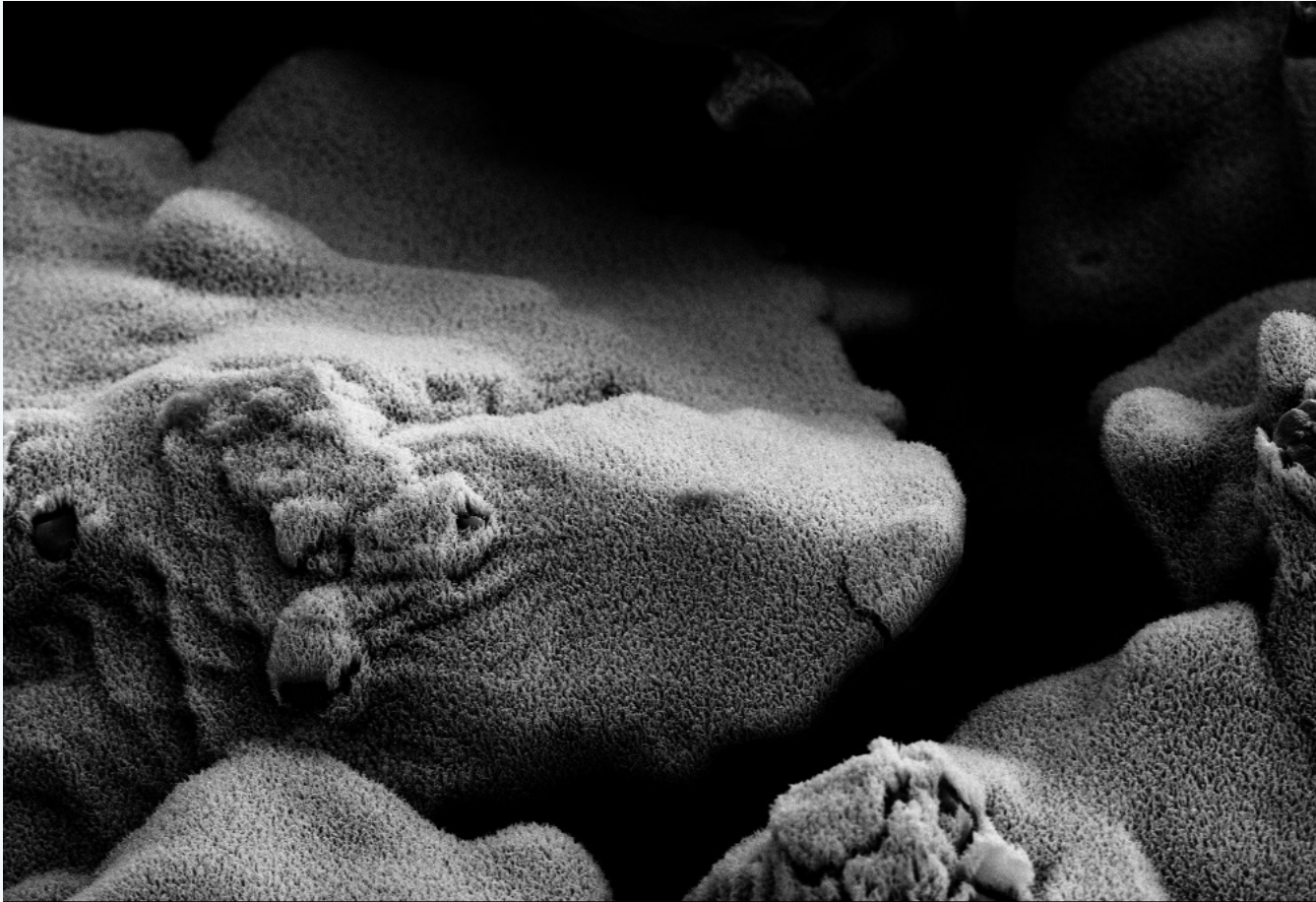
EDS mapping after 1000h





- Optimize the coverage and adhesion of ionomer towards PTE
- Initial catalyst activation protocol
- Match porosity parameters PTE – membrane e.g. extruded Nafion nanostructure
- **Modified PTL surface to work with thinner membranes**





-
- Now at $0.2 \text{ mg}_{\text{Ir}}/\text{cm}^2$:
 - Catalytic nanofiber substrate: 1000h at $2 \text{ A}/\text{cm}^2$ and up to 2.5V
 - Targets:
 - $2 \text{ A}/\text{cm}^2$ below 2V for 2000 hours
 - Prototype cells up to size A4
 - **Seeking Scale-Up Partners!**
-

Partner With Us – Raising Capital



- **Ellinor Ehrnberg**
President of Smoltek Hydrogen AB
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- **Fabian Wenger**
Head of R&D
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- **Shafiq Kabir**
Head of Volume Processes
shafiq.kabir@smoltek.com
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<https://www.smoltek.com/hydrogen/>





Backup Slides





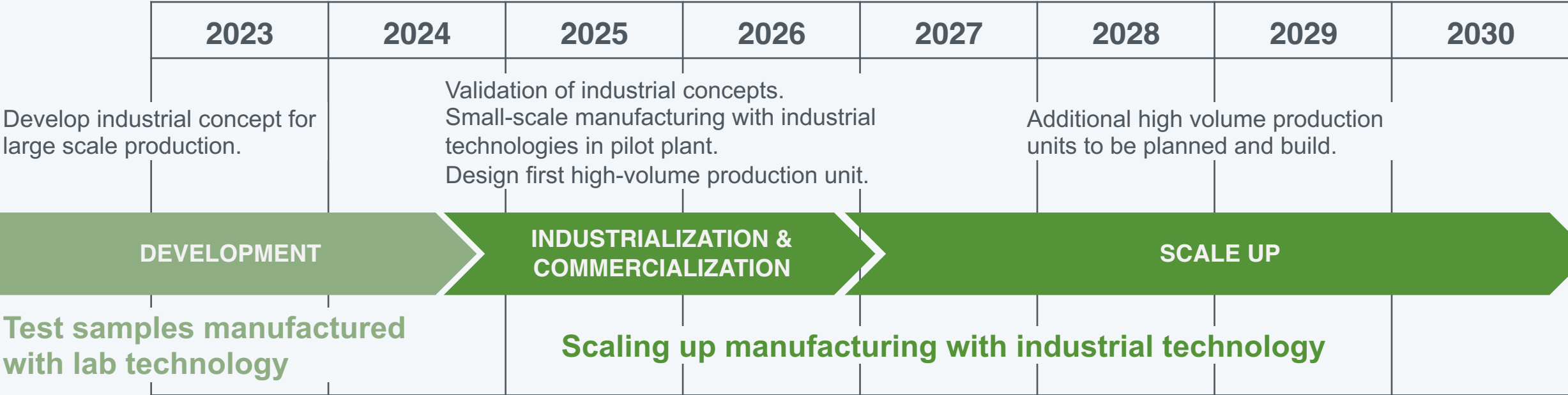
Shafiq Kabir
Head of Volume Processes

PhD in Microtechnology and Nanoscience, 2005

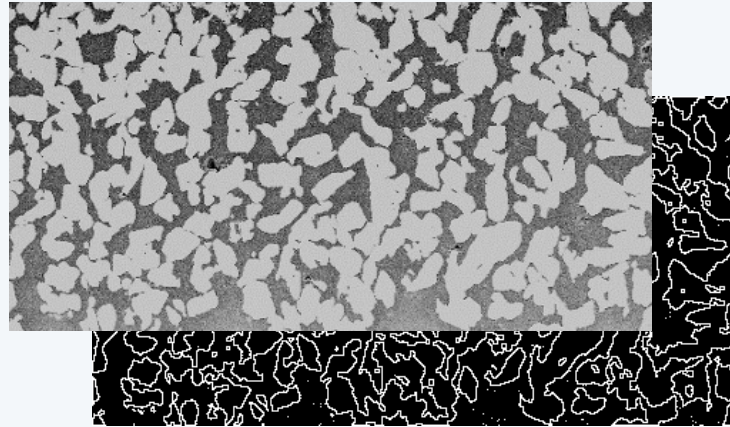


Réka Simon-Bálint
Head of Quality and Project Management

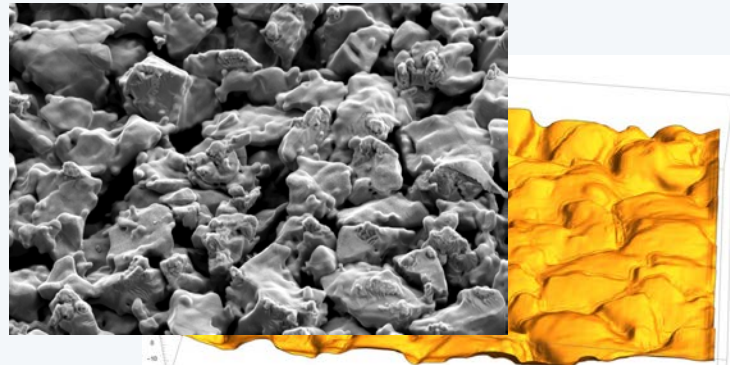
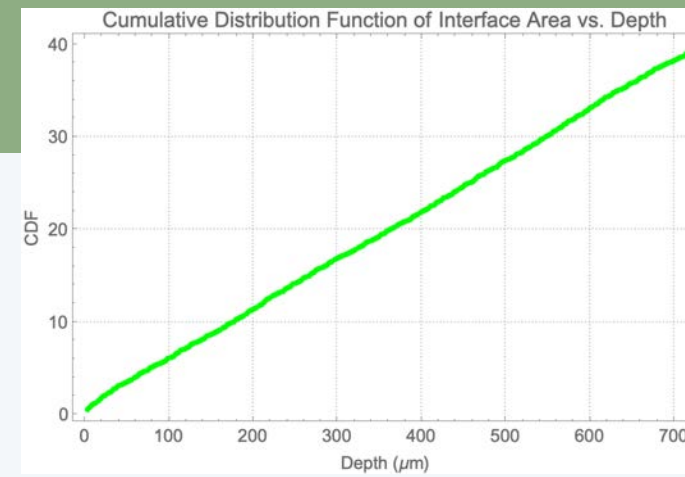
MSc in Physics & Materials, 2012



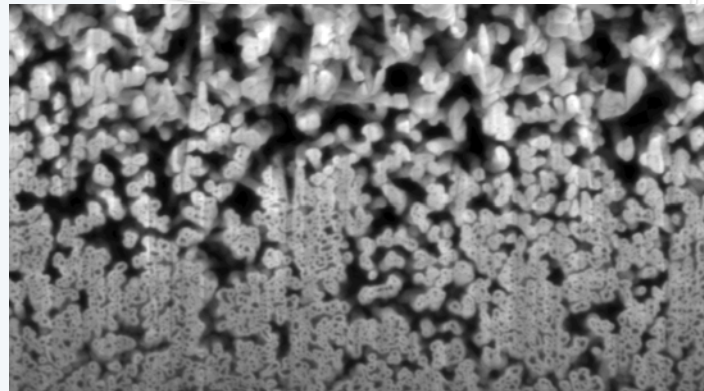
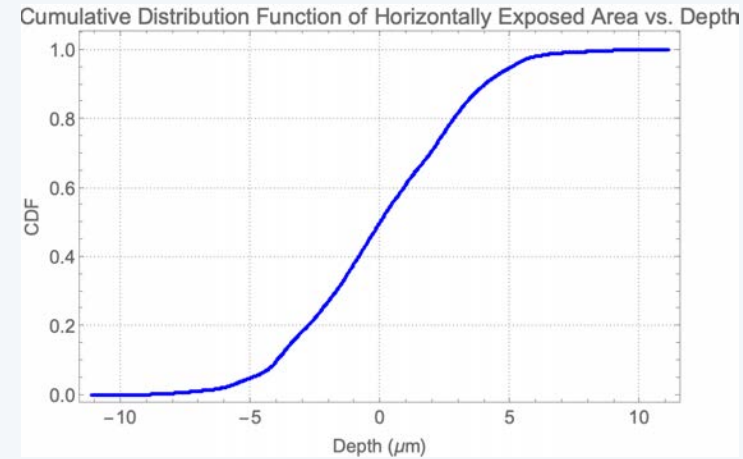
Active Area In Proximity To Ionomer



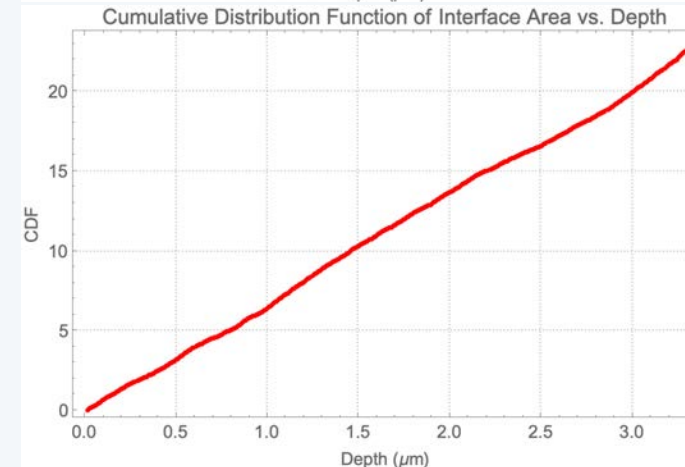
All layers of PTL

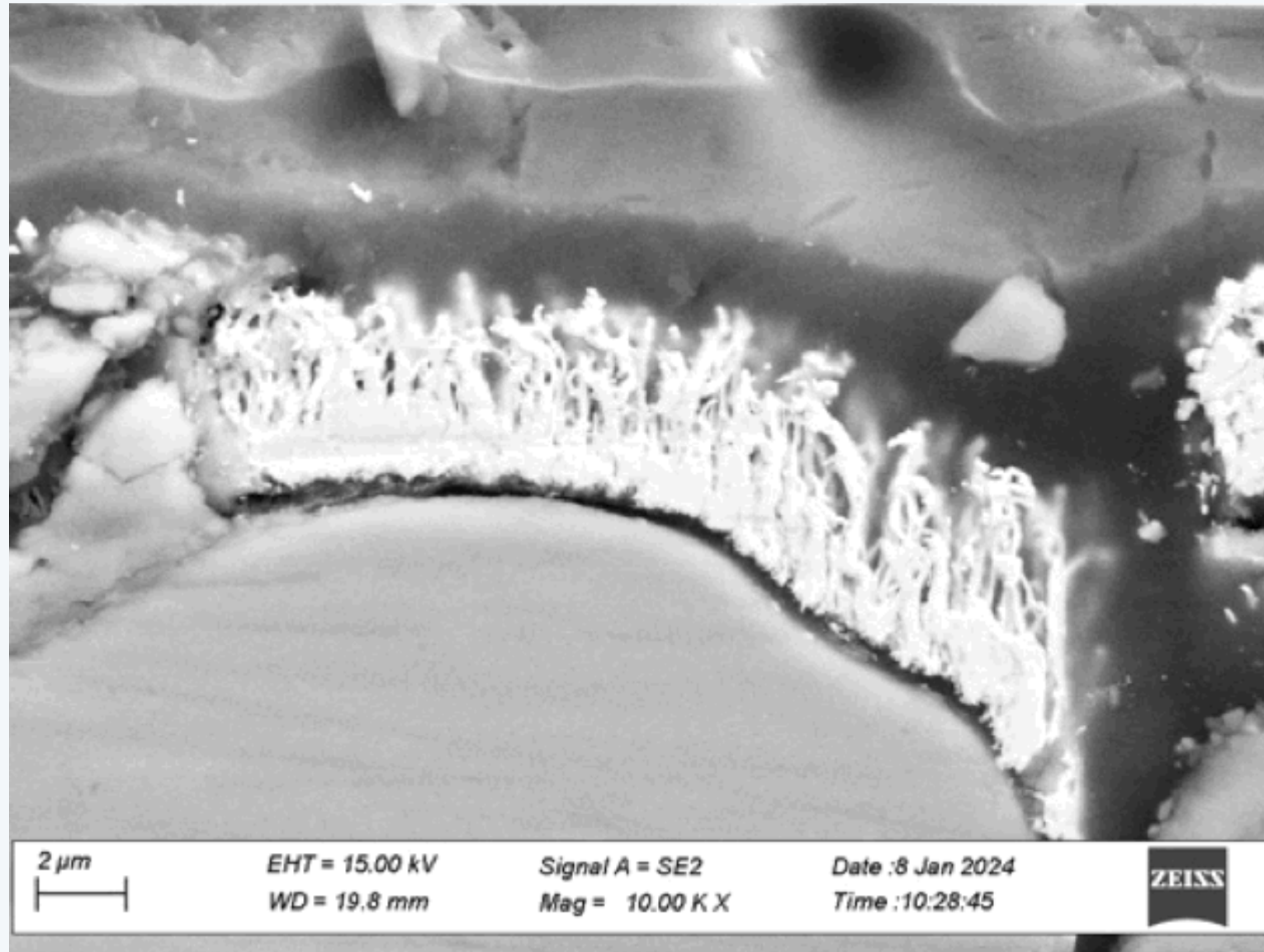
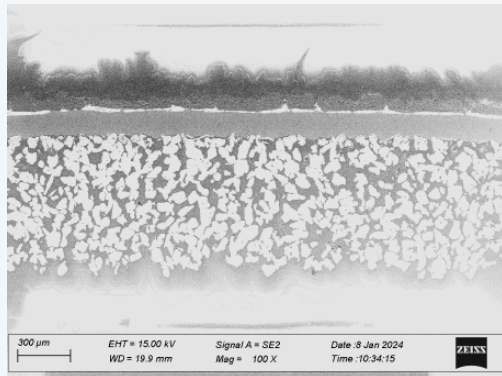


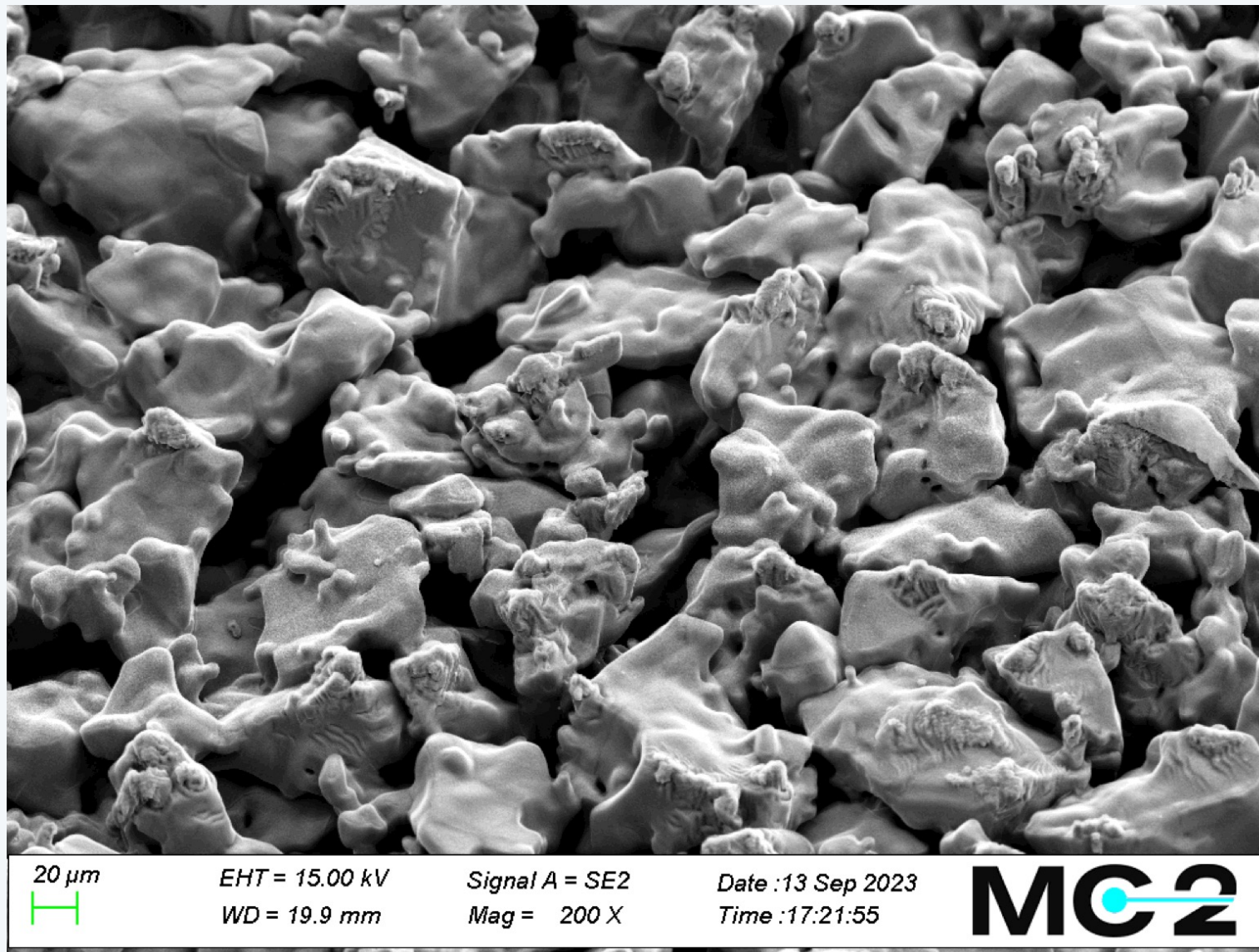
1st layer of PTL



Fiber Layer Depth

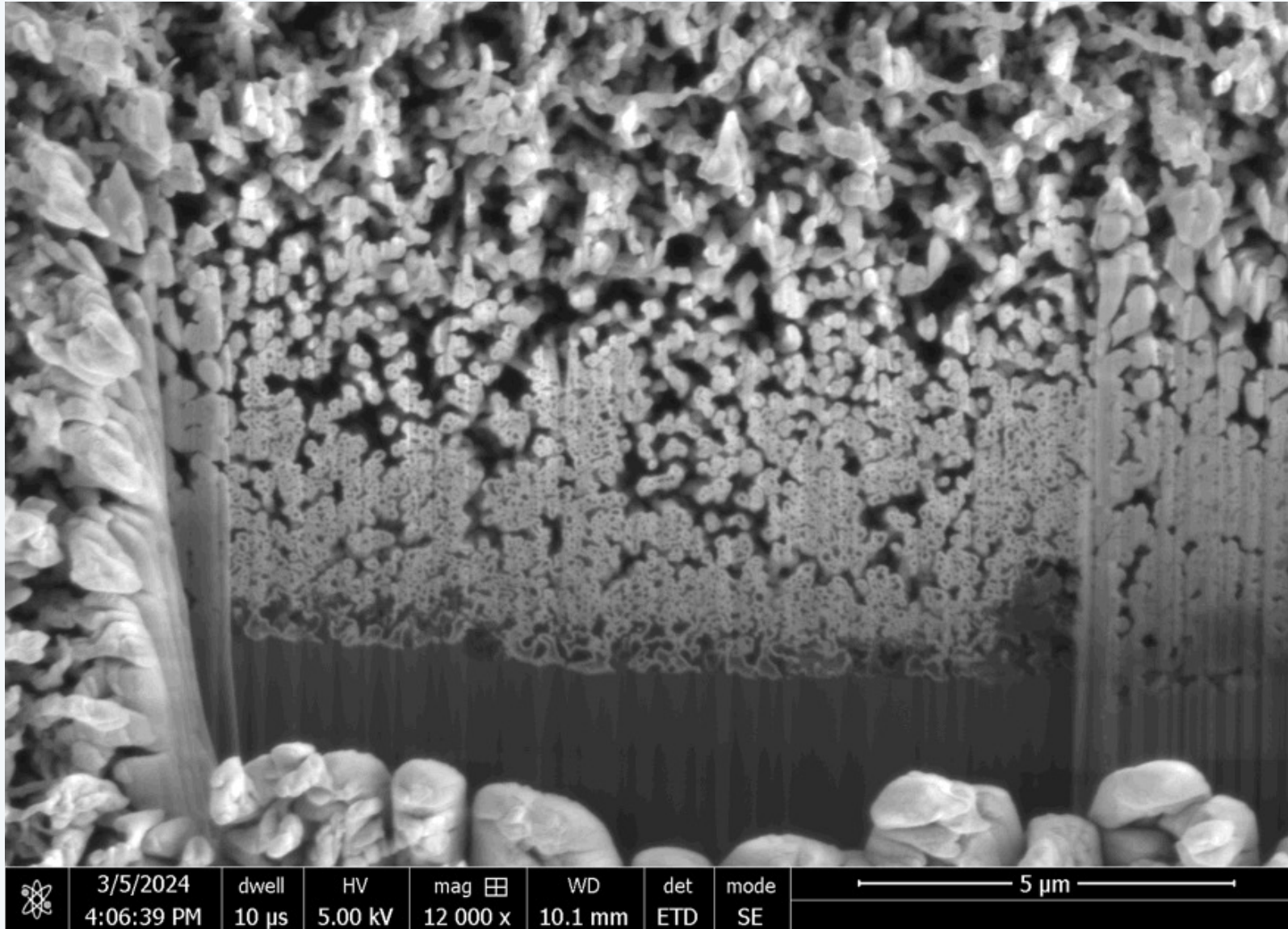




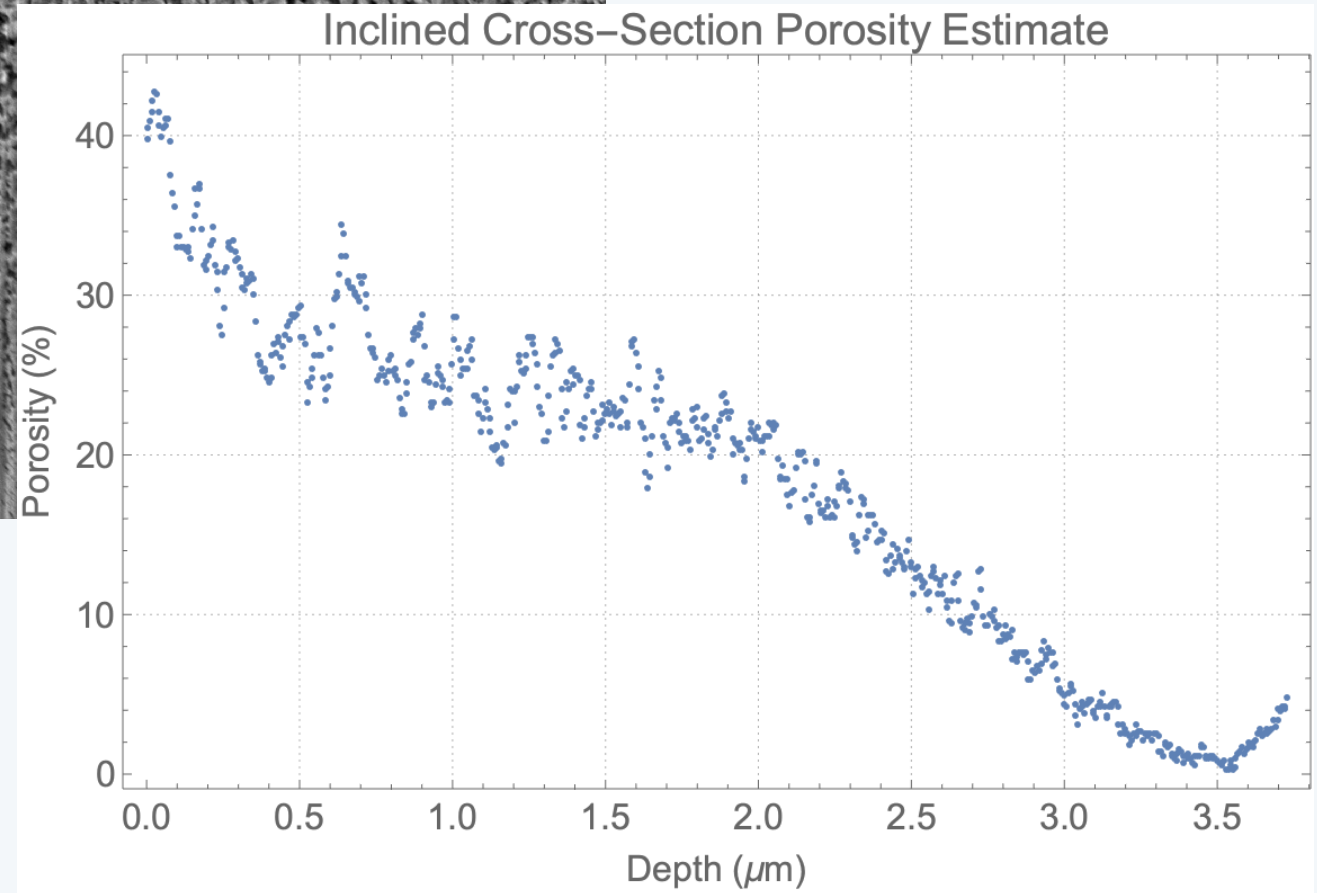
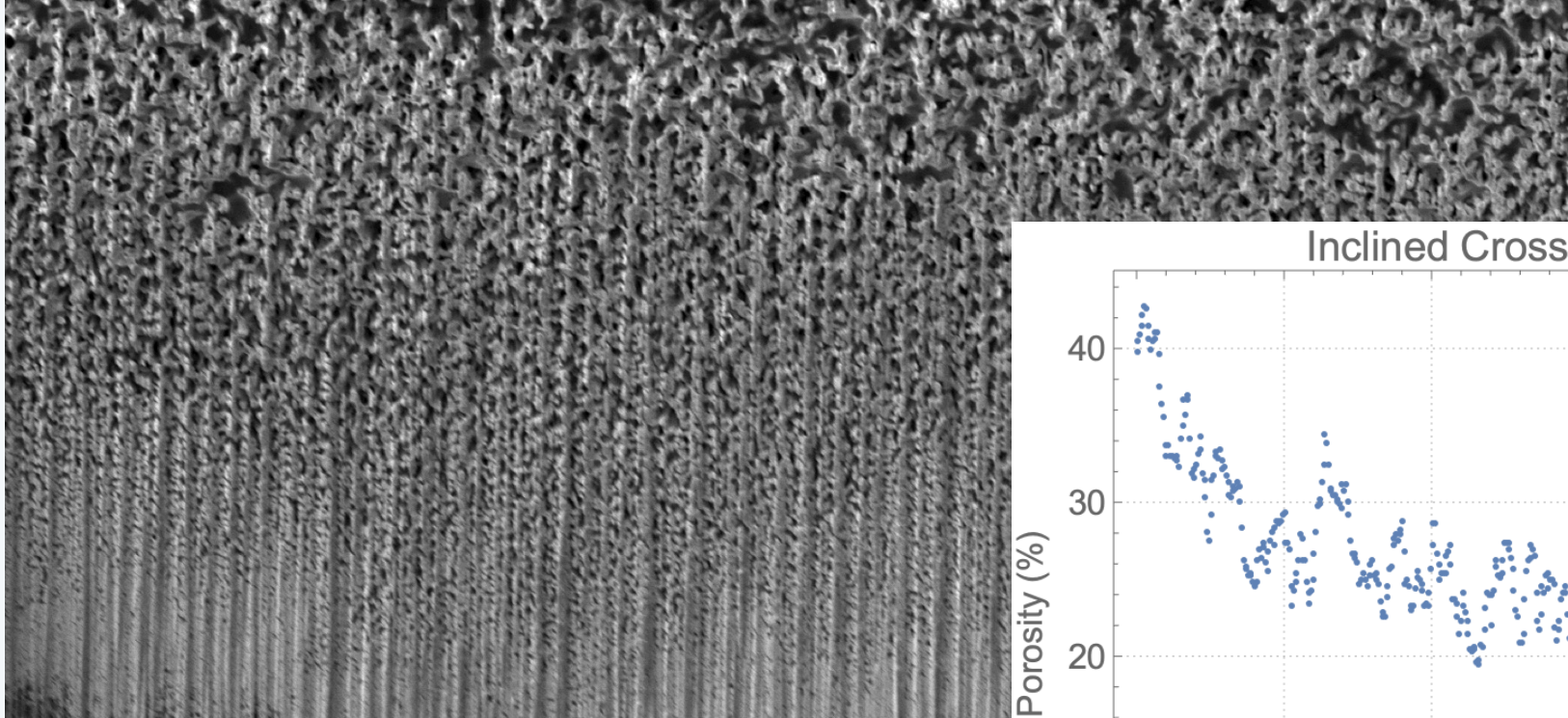




Collaborators:
Dylan Schulz,
Anna Martinelli

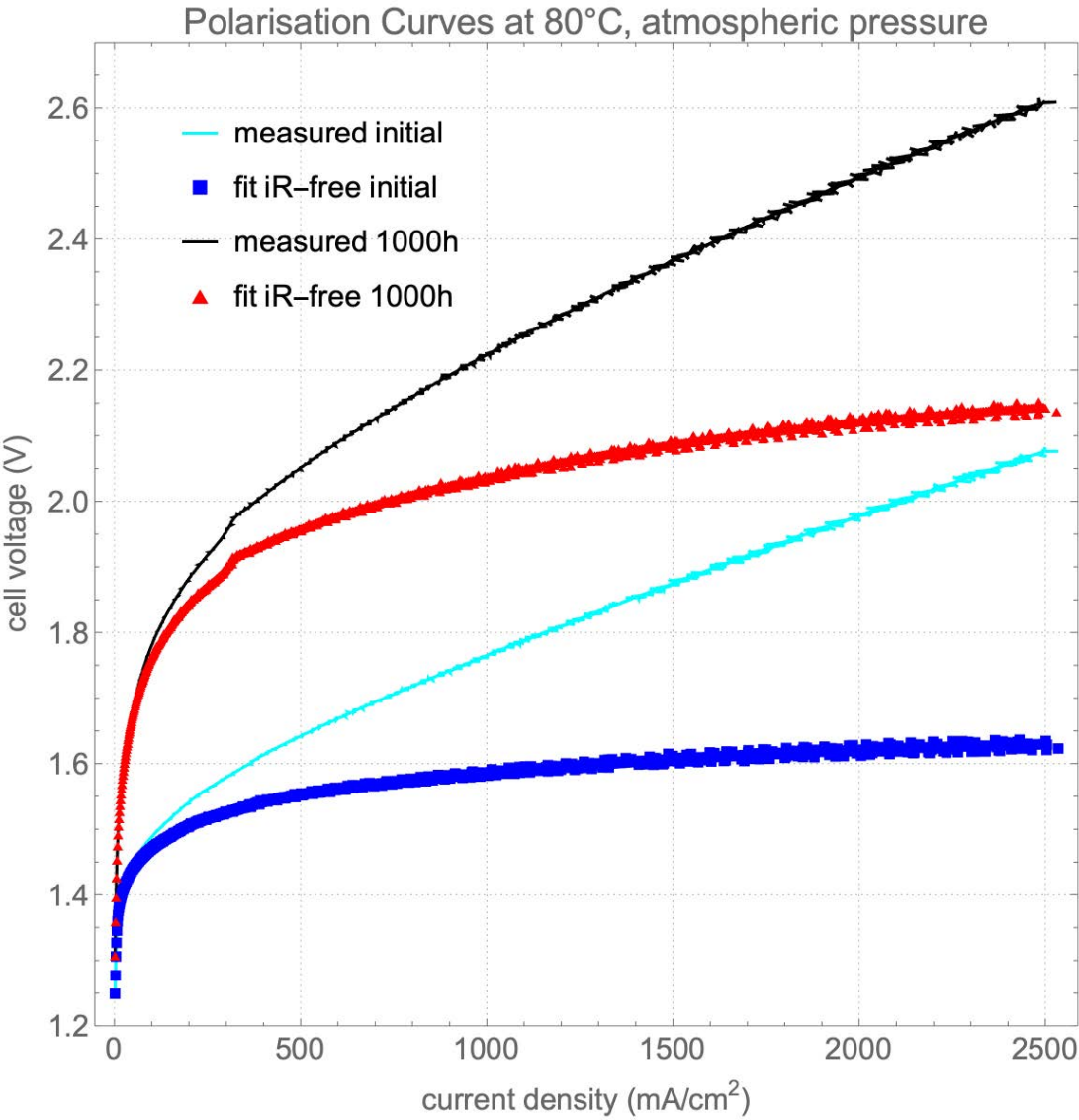


Smoltek Hydrogen AB



Swedish
Electricity Storage
and Balancing Centre

Collaborators:
Dylan Schulz,
Anna Martinelli



Electrocatalytic Oxygen Evolution Reaction (OER) on Ru, Ir, and Pt Catalysts: A Comparative Study of Nanoparticles and Bulk Materials

Tobias Reier,* Mehtap Oezaslan, and Peter Strasser

The Electrochemical Energy, Catalysis, and Materials Science Laboratory, Technische Universität Berlin, Department of Chemistry, 10623 Berlin, Germany

ABSTRACT: A comparative investigation was performed to examine the intrinsic catalytic activity and durability of carbon supported Ru, Ir, and Pt nanoparticles and corresponding bulk materials for the electrocatalytic oxygen evolution reaction (OER). The electrochemical surface characteristics of nanoparticles and bulk materials were studied by surface-sensitive cyclic voltammetry. Although basically similar voltammetric features were observed for nanoparticles and bulk materials of each metal, some differences were uncovered highlighting the changes in oxidation chemistry. On the basis of the electrochemical results, we demonstrated that Ru nanoparticles show lower passivation potentials compared to bulk Ru material. Ir nanoparticles completely lost their voltammetric metallic features during the voltage cycling, in contrast to the corresponding bulk material. Finally, Pt nanoparticles show an increased oxophilic nature compared to bulk Pt. With regard to the OER performance, the most pronounced effects of nanoscaling were identified for Ru and Pt catalysts. In particular, the Ru nanoparticles suffered from strong corrosion at applied OER potentials and were therefore unable to sustain the OER. The Pt nanoparticles exhibited a lower OER activity from the beginning on and were completely deactivated during the applied OER stability protocol, in contrast to the corresponding bulk Pt catalyst. We highlight that the OER activity and durability were comparable for Ir nanoparticles and bulk materials. Thus, Ir nanoparticles provide a high potential as nanoscaled OER catalyst.

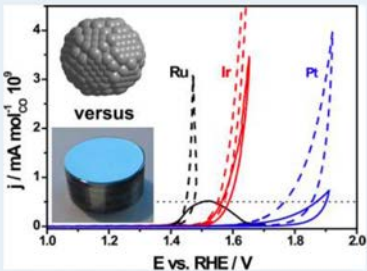
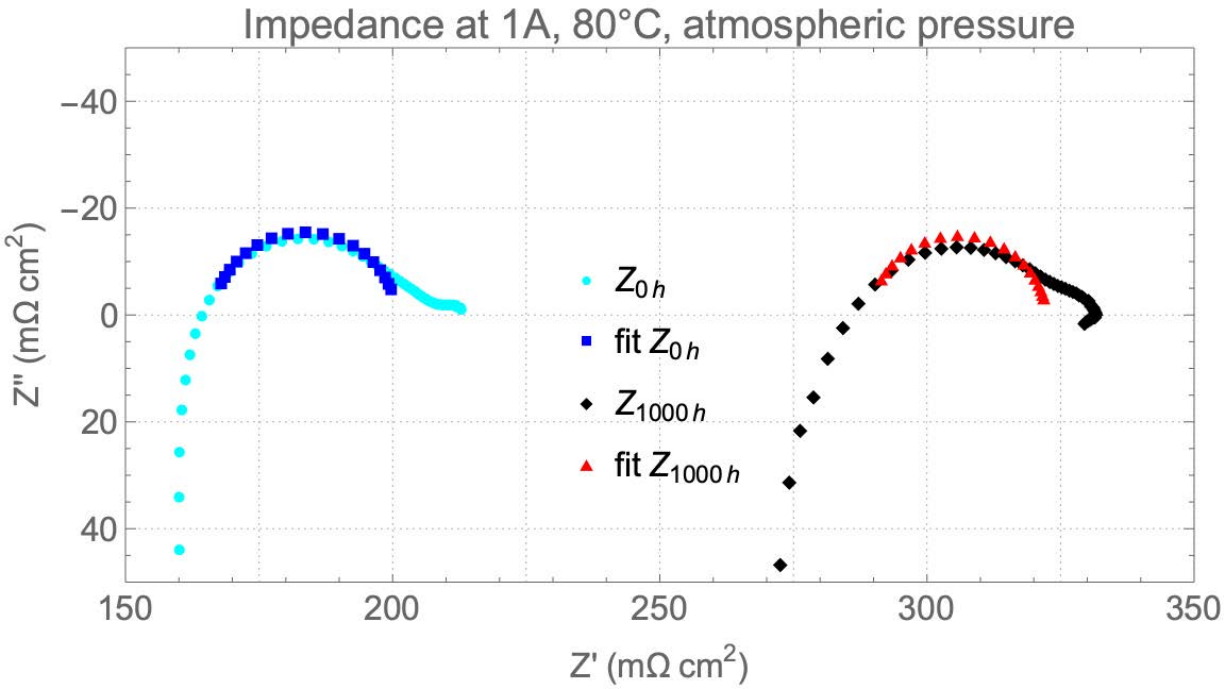


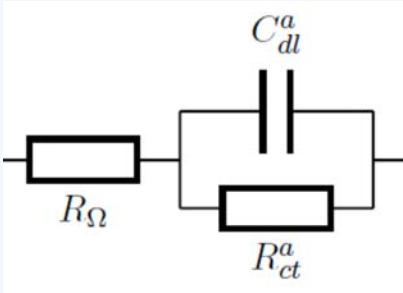
Table 3. Potentials for an OER Current Density of 0.5 mA mol⁻¹ 10⁹, Tafel Slopes, and Dissolved Metal Masses for Ir, Ru, and Pt Nanoparticle and Bulk Catalysts

catalyst	potential at 0.5 mA mol ⁻¹ 10 ⁹ /V		Tafel slope/mV dec ⁻¹		dissolved metal (ICP)/μg	
	bulk	nanoparticles	bulk	nanoparticles	bulk	nanoparticles
Ru	1.449	1.504	44		13.1 ± 0.2	1.7 ± 0.4
Ir	1.551	1.563	63	64	bld ^a	0.8 ± 0.3
Pt	1.766	1.870	145	210	bld ^a	bld ^a

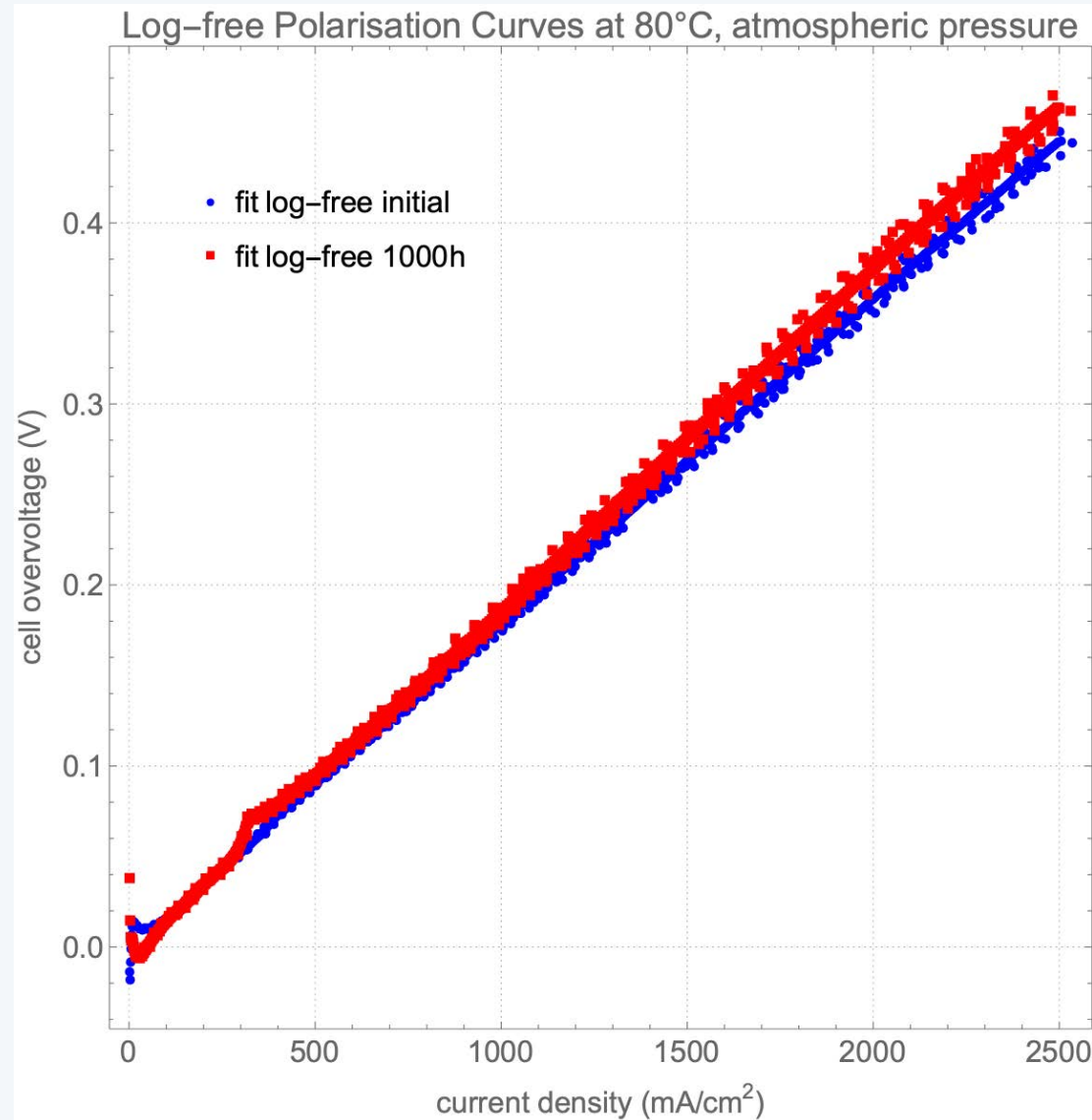
^abld - below limit of detection.

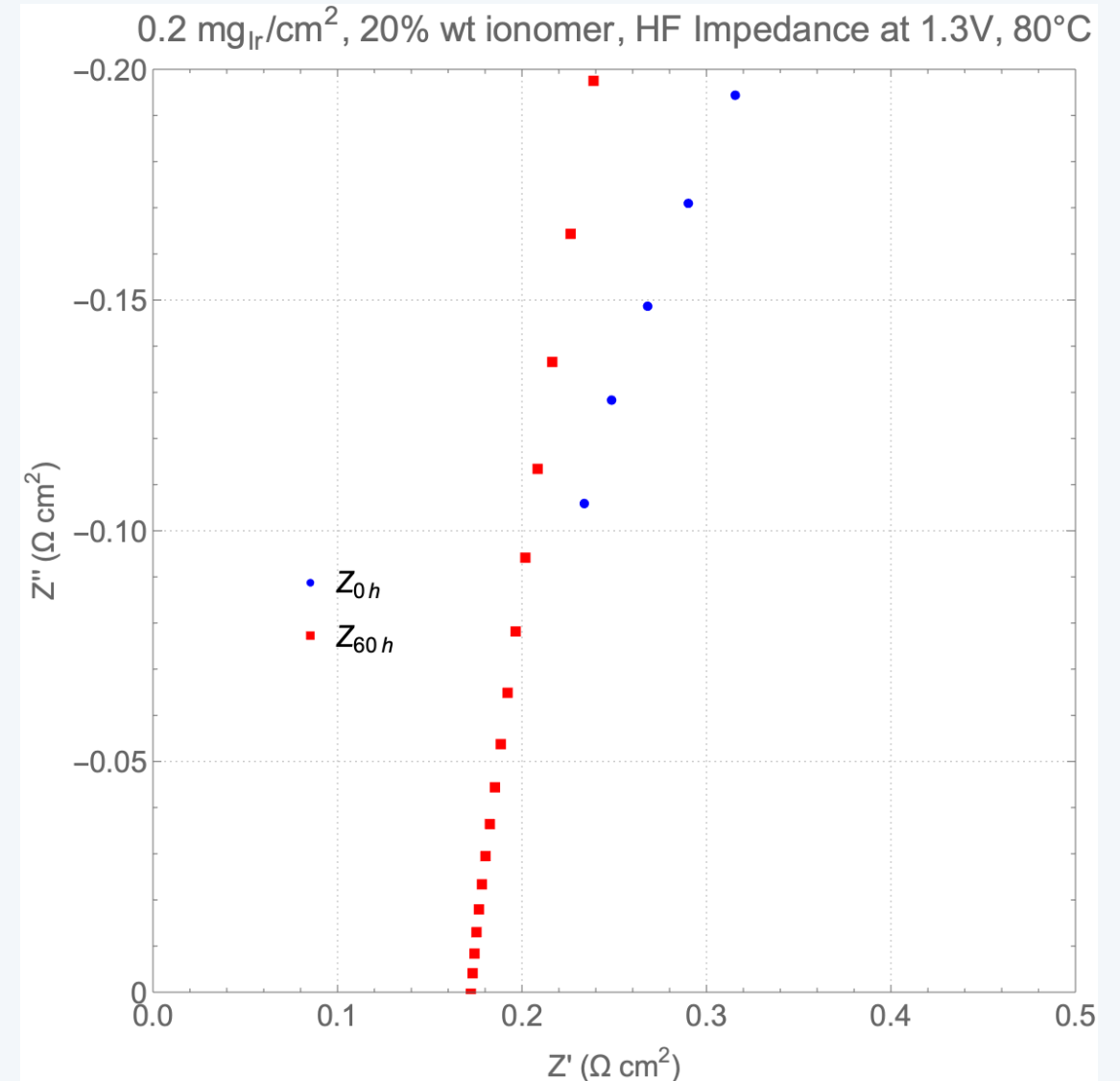
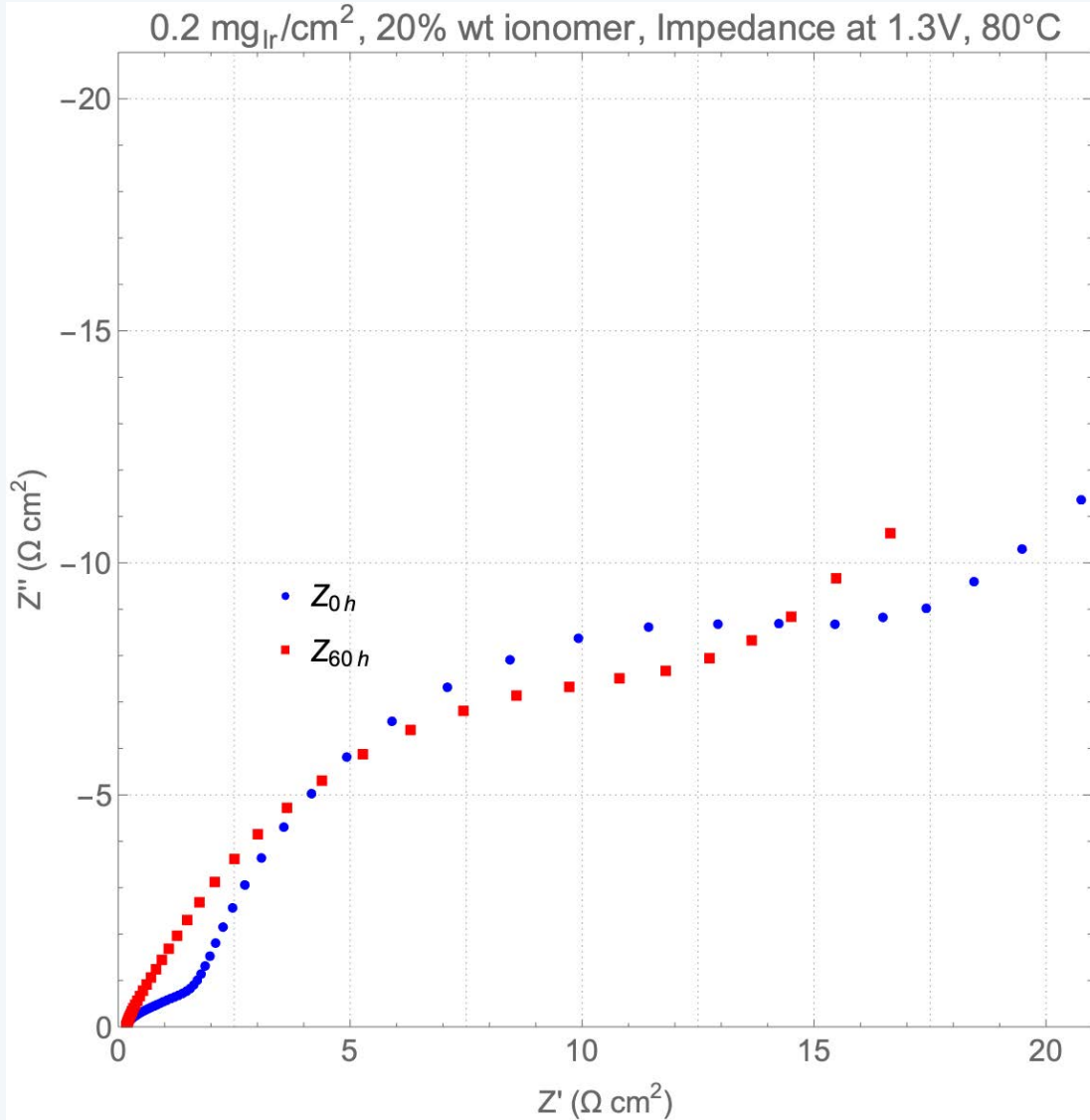


- EIS model simplified Randles circuit with CPE and non-linear fit of exponent in selected frequency interval



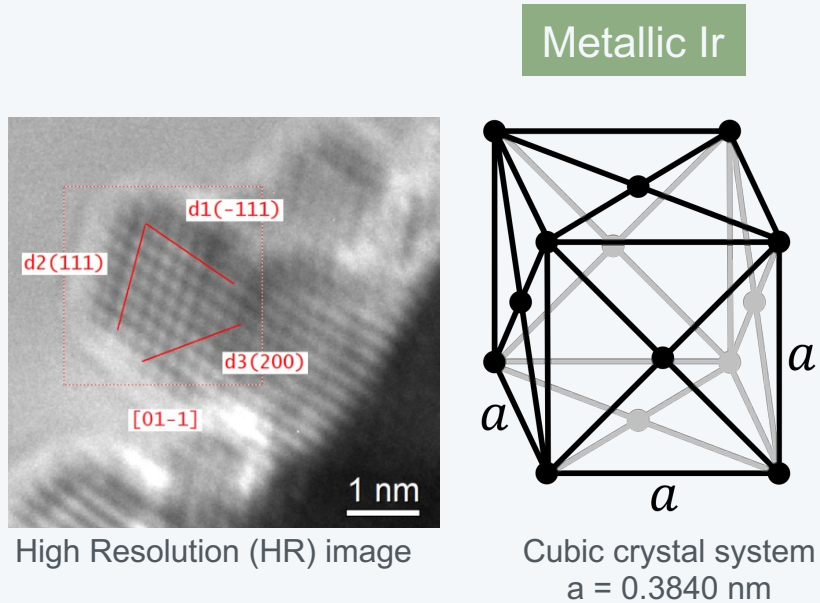
EIS @ 1A	HFR (mΩ cm ²)	R _{CT} (mΩ cm ²)	a	C _{CPE} (s ^{a-1} mF/cm ²)
0h	166	34	0.92	13
1000h	289	33	0.93	6





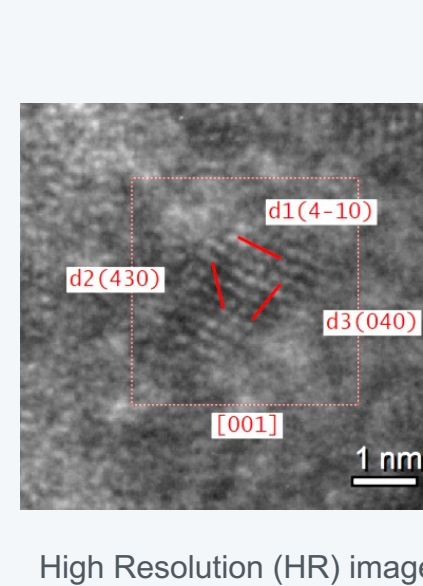
Before 1000h durability test

After 1000h durability test



d1 = 0.21637 nm
d2 = 0.21654 nm
d3 = 0.18940 nm
 $\angle d1d2 = 69.86^\circ$
 $\angle d2d3 = 53.31^\circ$

d(-111) = 0.2217 nm
d(111) = 0.2217 nm
d(200) = 0.192 nm
 $\angle d1d2 = 70.53^\circ$
 $\angle d2d3 = 54.74^\circ$



d1 = 0.2296 nm
d2 = 0.1817 nm
d3 = 0.2271 nm
 $\angle d1d2 = 52.79^\circ$
 $\angle d2d3 = 51.67^\circ$

d(4-10) = 0.2332 nm
d(430) = 0.1899 nm
d(040) = 0.2313 nm
 $\angle d1d2 = 52.62^\circ$
 $\angle d2d3 = 51.99^\circ$

